

Utilization Waste Brine Water Separator for Binary Electric Energy Conversion in Geothermal Wells

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Utilization Waste Brine Water Separator for Binary Electric Energy Conversion in Geothermal Wells

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ABSTRACT

Nowadays, geothermal is one of the most environmentally friendly energy that can replace the role of fossils energy by converting steam to electricity. Brine is one of the by-products of the production of geothermal wells that are generally not used or simply re-injected. In fact, brine can be converted into electricity using the binary cycle process. In binary cycle, brine from separator is used as a heater of working fluid and transform it into a vapour phase. The vapour will be used to turn turbines and generators to produce electricity. The working fluid selection in accordance with the heating fluid temperature becomes important because it results in optimization of the thermodynamic cycle. The temperature of the wellhead in the geothermal field will decrease 3% per year and reducing the heating fluid temperature in heat exchanger. So, in this paper intends to utilize brine to heat the heat exchanger by using iso-butane, n-pentane, and iso-pentane because its critical temperature can be stable at 193°C wellhead temperature. From the results of predictions from brain 2 production well for 17 years with iso-butane in this binary cycle planning, can utilize waste brine water separator to converse electric energy to produce 4 MWh electricity.

1. INTRODUCTION

In general, geothermal fields only use their steam by converting the steam to electricity. Brines that are produced with a high temperature, pressure, and mass flow rate can be used as electricity generation. Brine will only function as a heater of the working fluid. The working fluid used is a chemical compound that has a boiling point lower than the boiling point of water [1]. The heated working fluid vapors are later used to turn turbines and produce electricity.

Many working fluids can be used for binary cycle power plants. There have been many studies conducted to find out the most efficient working fluid applied to a power plant. Each working fluid must have basic characteristics, such as being able to produce high efficiency, as well as non-toxic, non-flammable, have low Global Warming Potential (GWP), do not have the potential to damage the ozone layer (ODP), and the cost is cheap [2]. Working fluids with high GWP such as chlorofluorocarbons (CFCs) were not included in this analysis. Refrigerants that contain chlorine or bromine can cause a decrease in the ozone layer. These components are unstable and when released into the atmosphere, they quickly go to the

uppermost atmosphere [3]. Another parameter that needs to be considered is the pressure of the working fluid, whether the pressure is condensation or evaporation. Some working fluids have large evaporative pressures such as isobutane and n-butane, which means they require extensive evaporators [4].

Working fluids which have high latent heat and high density are preferred. The working fluid absorbs more energy from its source in the evaporator. This will reduce the amount of fluid mass flow rate needed. Thus, resulting in the use of smaller generating facilities and pump power consumption [5]. There are three types of working fluids based on the slope of the saturated vapor line on the T-s diagram, namely dry, wet and isentropic fluids. Dry and isentropic working fluids produce better performance than wet fluids. The effect of boiling temperature on the thermal efficiency system is also considered. High-boiling work fluids have higher thermal efficiency [6]. In this study, dry working fluid is used and will be analyzed in the study, namely n-pentane, and iso-pentane, and iso-butane.

In previous studies, research on working fluids only choose the optimum working fluid for use in a field with particular condition. However, this study will discuss the prediction of the working fluid choice on the effect of wellhead temperature decline every year. The expected result is a working fluid suitable for use in certain wellhead temperature ranges. So that it can produce optimum electricity.

2. DATA AND FIELD STUDY

Binary cycle is a thermodynamic process where the main source is a hot fluid which is used to heat a working fluid through a heat exchanger [7]. The process of working fluid evaporation, usually called a closed cycle, is connected directly to the turbine as a power plant. The working principle of the binary cycle is that the brine from the production well will be flowed into one of the pipes in the heat exchanger to vaporize working fluids that have low boiling points such as

iso-butane, n-pentane, and iso-pentane. Steam produced by heating the working fluid in the heat exchanger is flowed to turn the turbine and then drive the generator to produce electricity.

The working fluid selection must be done in order to produce optimum energy. Thermodynamic analysis of the working fluid is also carried out in order to know the process that occurs in the working fluid during the binary cycle. After the thermodynamic cycle is known, the next step is to design the binary cycle.

Initially, the LHD Field will only utilize the steam produced to generate Steam Turbine. However, seeing the huge potential of brine seen from pressure, temperature, and mass flow, the Unit III LHD Field has the potential to build binary cycle power plant. The planned binary cycle scheme from Produced Well LHD-5 and LHD-19, is seen in Fig. 1.

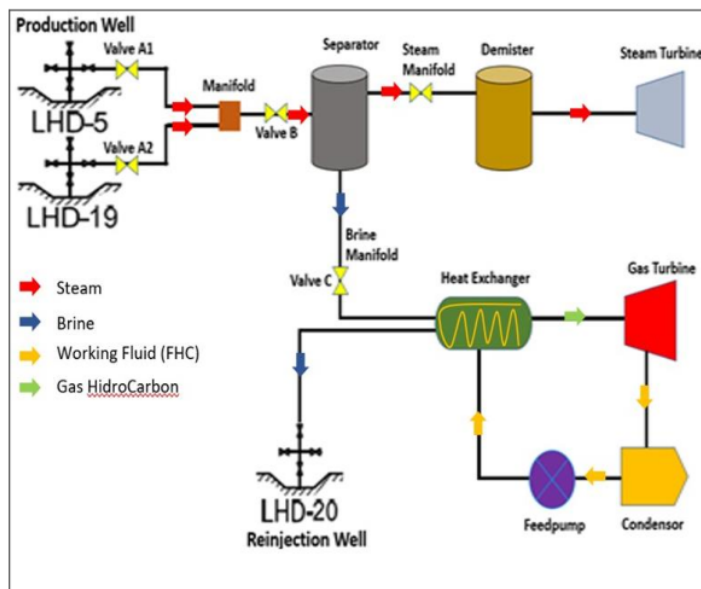


Figure 1. LHD Binary Cycle Scheme

3. METODOLOGY

This study is carried out in several stages:

3.1 Pressure and Temperature Loss Analysis and Pipe Dimension

Pressure and temperature loss calculations in the two-phase pipeline are needed because there might be losses in the pipeline. Later, the use of the Pipesim application is needed to calculate the pressure loss, temperature loss, and steam quality in the pipe. Equation from Beg and Brill to recommendation from to analysis pressure and heat loss 2 phase in pipe media.

Before calculating the amount of pressure loss and temperature loss in the two-phase pipe, it is necessary to determine the size of the pipe diameter to be used. Calculation of the dimensions of this pipe using the ASME standard. The steps in determining the dimensions of a pipe are as follows:

Determine the specific volume mixture between steam and brine using equation:

$$V_m = x \times V_v + (1-x) \times V_l \quad (1)$$

Determine a temporary Di (inner diameter) using equation:

$$Di = \frac{(m \times V_m)}{(1/4 \times \pi \times V)} \quad (2)$$

When :

V = Velocity (m/s)

m = Flow mass (kg/s)

V_m = Specific volume mixture (m³/kg)

Di = Inner diameter (m)

Determine pipe dimension or schedule based on calculated temporary inner diameter. Calculate minimum thickness of pipe and then validate it with pipe schedule from ASME standard and calculate flow velocity inside pipe.

3.2 Determining thermodynamic cycle of

each working fluid.

Determine Thermodynamics State of Working Fluid usually consist of 6 states based on the enthalpy and entropy curves of the working fluid to changes in pressure and temperature condition. The same thing is found. Generally, there are four processes in the binary cycle, namely isentropic in the feed pump, constant pressure adding heat to the heat exchanger, turbine isentropic expansion, and heat reinjection constant pressure in the condenser [4].

3.3 Calculating electrical power generated by turbine.

After knowing the thermodynamic state fluid cycle, and then calculating the mass flow rate of the working fluid using the following equation (3) :

$$m_{wf} = \frac{m_b \times c_b \times (T_A - T_B)}{h_1 - h_6} \quad (3)$$

Assuming $\Delta T_{pp} = 5$ K (specification of the tools used), then :

$$T_B = T_6 + 5 \text{ K} \quad (4)$$

When :

m_{wf} = The mass flow rate of the working fluid (kg/s)

m_b = Brine flow rate (kg/s)

T_A = Brine Temperature (K)

T_B = Brine Temperature out (K)

h_1 = Enthalpy of incoming working fluid (kJ/kg)

h_2 = Enthalpy of the working fluid out (kJ/kg)

T_6 = Temperature at state 6 (K)

To calculate the electric power produced, can use the following equation :

$$\dot{W}_t = \dot{m}_{wf} \times \eta_t \times (h_3 - h_{4s}) \quad (5)$$

When :

W_t = The electric power is generated (kWe)

M_{wf} = The mass flow rate of the working fluid (kg/s)

H_t = Turbine efficiency (%)
 $h_{3&4}$ = Enthalpy inlet & outlet Turbine (kJ/kg)

equation :
 $Q_m = h_1 - h_5$ (8)

3.4 Efficiency Cycles Thermal

To find out the specific performance of the turbine needed, equations can be used ;

$W_t = h_1 - h_2$ (6)

Working specification of Feed pump , the equation can be used :

$W_p = h_5 - h_4$ (7)

The heat transfer working fluid, can be used

Thermal efficiency is the ratio of the net power generated by the head bed applied to a system. This value show how much power can be produced with a certain heat input . Thermal efficiency can be calculated using the equation :

$\eta_{th} = \frac{[W_t - W_p]}{q_{in}}$ (9)

4.RESULT AND DISCUSSION

4.1. Determnation of Pressure and Temperatur Loss

Initially, the LHD Unit III Field will only utilize the steam produced. However, seeing the huge potential of brine seen from pressure, temperature, and mass flow, the Unit III LHD Field has the potential to build binary cycle power plant. In accordance with the plan, the LHD-5 and LHD-19 merupakan sumur dalam satu cluster yang dibor pada stuktur yang sama sehingga memiliki karakteristik dan produksi yang relatif sama. dan direncanakan will be constructed with a binary cycle power plant. The two wells will be distributed to a singleler. Then from the separator, the brine will flow

exchanger.

In the heat exchanger there is heat transfer between the produced brine and the working fluid.

Working fluid which has changed phase into gas will be directly used to rotate the gas turbine. The working fluid that has been used is then condensed in the condenser to return the phase to liquid. This liquid is then pumped back to the heat exchanger to be reheated by the produced brine. This cycle continues. **Table 1A** , to explain well output data from LHD-5 and LHD-19 Well and Table 1A. dimation pipe to Manifold and

Table 1A , Well output data LHD-5 and LHD-19 Well

Well Data	Well Output	
	LHD-5	LHD-19
Fluid	2 Phase	2 Phase
Temperature (°C)	193	193
Pressure (bar)	13.4	13.4
Mass Flow (kg/s)	50.399	50.399
Steam Quality (%)	20	20
Enthalpy (kJ/kg)	1214.7	1214.7

Table 1B. Dimension Pipline From Well-Manifol and Separator

Well to Manifold	Inside Diameter (inch)	11.75	11.75

through the brine manifold to the heat

to Separator

	Outside Diameter (inch)	12.75	12.75
	Pipe Thickness (inch)	0.5	0.5
Manifold to Separator Pipeline Dimension	Inside Diameter (inch)	15	
	Outside Diameter (inch)	16	
	Pipe Thickness (inch)	0.5	

Fluid Flow 2 phase from Production Well (LHD-5 and LHD-19) to Manifold and Separator and Single phase fluid (Brine) from Separator to Head Ex changer. Well output data from each well, LHD-5 and LHD-19 are attached in Table- I. The data will need to be corrected by the pressure and temperature losses that occur along the pipe so that the separator output brine data will be obtained, which will be used for the calculation of this study. The flow from well to separator in the 2-phase pipeline causes pressure and temperature loss which will affect the quality of steam and enthalpy. The pressure and temperature loss are analyzed using the Pipesim simulator. The assumption using proper insulation so that the heat loss does not spread to the pipe surface and only calculates the

loss of pressure and temperature along the 2-phase pipeline, as shown in Table 2, Table 3. Pressure and temperature loss data in to phase (Liquid dominated system) from Production Well (LHD-5 and LHD-19) to Manifold, can show in Table 2 A and Table 2B. The pressure and temperature loss in two-phase (liquid Dominated) from Manifold to Separator as follow in Table 3A and Table 3B. Evaluation of value presurre dan temperatur loss single phase (Brine) from Sepator to Head Exchanger to show in Table 4.

Table 2 A. Pressure and Temperature

Well	Wellhead		Loss Through Well-Inlet Valve A ₁ /A ₂		Inlet Valve A ₁ /A ₂		Loss in Valve A ₁ /A ₂	
	P (bar)	T (°C)	P (bar)	T (°C)	P (bar)	T (°C)	P (bar)	T (°C)
LHD-5	13.4	193	0.0726	0.249	13.3274	192.75	0.000219	0
LHD-19	13.4	193	0.0726	0.249	13.3274	192.75	0.000219	0

Loss in Two-Phase , From LH5 and LHD-19 to Manifold

Table 2B. Pressure and Temperature Loss in Two-Phase , From LH5 and LHD-19 to Manifold

Well	Outlet Valve A ₁ /A ₂		Loss Through Outlet Valve A ₁ /A ₂ -Inlet Manifold		Inlet Manifold	
	P (bar)	T (°C)	P (bar)	T (°C)	P (bar)	T (°C)
LHD-5	13.3272	192.75	0.216681	0.757	13.111	191.99
LHD-19	13.3272	192.75	0.216681	0.757	13.111	191.99

Table 3A. Pressure and Temperature Loss in Two-Phase From Manifold to Separator

Outlet Manifold		Loss Through Outlet Manifold-Inlet Valve B		Inlet Valve B		Loss in Valve B		Outlet Valve B	
P (bar)	T (°C)	P (bar)	T (°C)	P (bar)	T (°C)	P (bar)	T (°C)	P (bar)	T (°C)
13.1	191.99	0.065	0.23	13.0453	191.765	0.000235	0.001	13.04506	191.764

Table 3B. Pressure and Temperature Loss in Two-Phase From Manifold to Separator (B)

Loss Through Outlet Valve B-Inlet Separator		Inlet Separator		Loss Inside Separator		Outlet Separator		Loss Through Outlet Separator-Inlet Valve C	
P (bar)	T (°C)	P (bar)	T (°C)	P (bar)	P (bar)	P (bar)	T (°C)	P (bar)	T (°C)
1.264665	4.64	11.7804	187.124	0.0136	0.0136	10.3	181.166	0.0136	0.057

Table 4. Pressure and Temperature Loss in Single-Phase Braine From Separator to Heat Exchanger

Outlet Separator		Loss Through Outlet Separator-Inlet Valve C		Inlet Valve C		Loss in Valve C		Outlet Valve C		Loss Through Outlet Valve C-Inlet Heat Exchanger		Inlet Heat Exchanger	
P (bar)	T (°C)	P (bar)	T (°C)	P (bar)	T (°C)	P (bar)	T (°C)	P (bar)	T (°C)	P (bar)	T (°C)	P (bar)	T (°C)
10.3	181.166	0.0136	0.057	10.2864	181.109	0.0005	0.002	10.2859	181.107	0.0559	0.238	10.23	180.869

The amount of pressure loss and temperature of fluid flowing from the LHD-5 well to the manifold through a pipe with an outer diameter of 12.75 inches and the length of the pipe is assumed to be 40 m is 0.29 bar for pressure loss and 0.023 °C for temperature loss. From the LHD-19 well to the manifold through a pipe with an outer diameter of 12.75 inches and a pipe length assumed to be 40 m is 0.2 bar for pressure loss and 0.03 °C for temperature loss. From the manifold to the separator inlet also experiences pressure and temperature loss. Outlet pressure and temperature data used in the manifold are the smallest data between LHD-5 and LHD-19 wells. The amount of pressure loss

and temperature of the fluid from the manifold to the separator inlet that flows in a 16 inches outer diameter pipe assuming a pipe length of 210 m is 1.31 bar for pressure loss and 0.08 °C for temperature loss. Inside the separator also occurs a pressure loss of 1.57 bar and 12.1 °C for temperature loss. So, the output data for brine separator is temperature of 180.8 °C, pressure of 10.23 bar, mass flow rate of 82.05 kg/s, enthalpy of 766.89 kJ/kg, and steam quality of 0% with the assumption of separation in the separator is perfect.

Well Data	Well Output		Manifold	Inlet Separator	Outlet Separator
	LHD-5	LHD-19			
Fluid	2 Fasa	2 Fasa	2 Fasa	2 Fasa	1 Fasa (Brine)
Temperature (°C)	193	193	192.97	192.896	180.8
Pressure (bar)	13.4	13.4	13.175	11.865	10.23
Mass Flow (kg/s)	50.399	50.399	100.798	100.798	82.05
Steam Quality (%)	20	20	19.75	18.6	0
Enthalpy (kJ/kg)	1214.7	1214.7	1210.48	1187.34	766.89

Thus, tabulation for each fluid data from the LHD-5 and LHD-19 wells on each nodal that has been corrected with pressure and temperature loss, shown in Table 5.

Table 5. Fluid Data in Each Nodal

The pipe planning 1-phase also needs to be done to find out how much the pipe diameter passed by the fluid and the fluid flow velocity in the pipe. This 1-phase pipeline plan includes a separator to heat exchanger segment, a heat exchanger to

turbine segment, a turbine to condenser segment, a condenser to feed pump segment, and a feed pump to heat exchanger segment. Pipe Schedule and Fluid Velocity for 1-Phase Pipeline can be seen in the Table 6.

Table 6. Pipe Schedule and Fluid Velocity for 1-Phase Pipeline

Pipe	Separator to HE	HE to Turbine	Turbine to Condenser	Condenser to Feed Pump	Feed Pump to HE
Di (inch)	9.75	23	5.762	1.938	1.938
Do (inch)	10.75	24	6.626	2.374	2.374
S (inch)	0.5	0.5	0.432	0.218	0.218
Fluid Velocity (m/s)	1.92	27.67	21.675	20.353	19.7

In this plan, the type used is A106 Grade B type carbon steel, XS (Xtra Strong) type because this type can be used in high temperature and high pressure conditions, making it suitable for geothermal fields. Table- IV. is a calculation on each pipe segment to determine the pipe schedule according to ASME B36.10M standard and the flow velocity in the pipe.

The pipe segment from the LHD-5 well to the manifold uses a pipe with Di (inner diameter) of 11.75 inch, Do (outer diameter) 12.75 inch, and s (pipe thickness) of 0.5 inch. The 2-phase fluid rate of steam and brine flowing in this segment is 24.565 m/s. The pipe segment from well LHD-19 to the manifold uses pipes with Di (inner diameter) of 11.75 inch, Do (outer diameter) of 12.75 inch, and s (pipe thickness) of 0.5 inch. The 2-phase fluid rate of steam and brine flowing in this segment is 26.338 m/s. The pipe segment from the manifold to the separator uses pipes with 15 inches, 16 inches, and 0.5 inches. The 2-phase fluid rate of steam and brine flowing in this segment is 26.98 m/s. The pipe segment from the separator to the heat exchanger has dimensions of 9.75 inch, Do 10.75 inch, and s of 0.5 inch. Brine fluid flow rate of 1.92 m/s. The pipe segment from the heat exchanger to the turbine has dimensions of 23 inches, 24 inches and 0.5 inches. Working fluid flow rate of 27.67 m/s. The pipe segment from the turbine to the condenser has dimensions at 5.762 inches, Do 6.626 inches, and s at 0.432 inches. Flow rate of working fluid flowing at 21,675 m/s. The pipe segment from the condenser to the feed pump has dimensions at 1.938 inches, Do 2.374 inches, and s at 0.218 inch. The flow rate of working fluid flowing at 20.353 m/s. The pipe segment from

the feed pump to the heat exchanger has dimensions of 1.938 inch, Do 2.374 inch, and s of 0.218 inch. Flow rate of working fluid flowing at 19.70325 m/s.

The wellhead temperature will decrease each year because the ability to produce geothermal fluid will also decrease annually. The decrease in wellhead temperature will also affect the decrease in the brine temperature entering the heat exchanger. With the prediction for over 17 years, from 2020 to 2036 and the reduction in wellhead temperature by an average of 3% / year, the annual temperature reduction can be seen in Fig. 3.

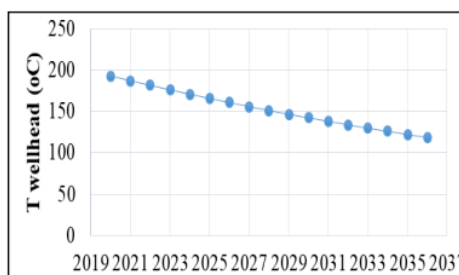


Figure 3. Temperature Decline Every Year (From 2019-2037)

4.2. Working Fluid Selection an Design

Working fluids from hydrocarbons were used, namely iso-butane, iso-pentane, and n-pentane , Working Fluid Characteristic can as Show n Table 7.

Table 7. Working Fluid Characteristic [9]

Fluid	Formula	Critical temp. (°C)	Critical pressure (bar)	Molar mass (kg/kmol)	Toxicity	Flammability	ODP*	GWP**
Propane	C ₃ H ₈	96.95	42.36	44.09	Low	very high	0	3
i-Butane	i-C ₄ H ₁₀	135.9	36.85	58.12	Low	very high	0	3
n-Butane	n-C ₄ H ₁₀	150.8	37.18	58.12	Low	very high	0	3
i-Pentane	i-C ₅ H ₁₂	187.8	34.09	72.15	Low	very high	0	3
n-Pentane	n-C ₅ H ₁₂	193.9	32.40	72.15	Low	very high	0	3
R-12	CCl ₂ F ₂	112.0	41.14	120.9	non-toxic	non-flam.	1.0	4,500
R-114	C ₂ Cl ₂ F ₄	145.7	32.89	170.9	non-toxic	non-flam.	0.7	5,850
R134a	CH ₂ FCF ₃	101.0	40.59	102.0	Low	non-flam.	0	1,430
R254fa	C ₃ H ₂ F ₃	154.0	36.51	134.0	Low	non-flam.	0	1030
Ammonia	NH ₃	133.6	116.27	17.03	Toxic	Lower	0	0
Water	H ₂ O	374.1	220.89	18.02	non-toxic	non-flam.	0	-

The wellhead temperature which decreases every year will

require changes in the working fluid as well, so that the electrical power produced remains optimum. Table 5, is a characteristic table of several working fluids. In this study only three working fluids from hydrocarbons were used, namely iso-butane, iso-pentane, and n-pentane which are attached in Table 8. The selection is based on the binary cycle equipment used, namely the gas turbine, so that the working fluid used comes from hydrocarbons. In addition, the three working fluids have critical temperatures that match into the wellhead temperature range of 193-119 °C. The other hydrocarbon fluids in Table 5, are not used because they have a critical temperature that is too low so that excessive evaporation will occur and cause the turbine not to rotate optimally, it is also possible for the turbine to burn and produce a non-optimum binary cycle. The working fluid of refrigerants is also not used because it has a high GWP (Global Warming Potential), so that it will damage the environment.

Tabel 8. Chosen Working Fluid Properties

For the iso-butane maximum allowable temperature is 125 °C and critical temperature is 134.7 °C as attached in Table 6. The iso-pentane has maximum allowable temperature of 177 °C and critical temperature of 187.2 °C. Whereas the n-pentane has a maximum allowable temperature of 186 °C and a critical temperature of 196.5 °C. The next step is to analyze the thermodynamic cycle. It is important to calculate how much energy is produced.

4.3. Thermodynamic State of Fluid Working HC

Thermodynamic state from Working fluid is condition Pressure, Temperature Entalphy and Entrophy in binary cycle process. Ada 8 state dari fluida kerja di dalam cyclus biner ini, yaitu : State 1 (Turbin), State 2 (Turbin output) , State 2s (kondisi isotropic pada outlet turbin), State 2 (kondisi outlet turbin), , State 3, State 4 (feed

pump), state 5, state 5s dan state 6. Thermodynamics State of iso-butane dapat dilihat pada Table 9.

State 1 : Vapour Saturated , at $P = 2 \text{ MPa}$
 $s_1 = 2.0735 \text{ kJ/kg K}$
 $h_1 = 642.378 \text{ kJ/kg}$

State 2: Use Equation Turbine Efficiency, $P = 0.53 \text{ MPa}$
 $h_2 = h_1 - \eta_t (h_1 - h_2) = 582.875 \text{ kJ/kg}$

State 2s: Isotropic Condition With state 1
 $s_{2s} = s_1 ; P_{2s} = P_{cond.}$
 Interpolasi s pada $T = 372.5 \text{ K}$
 $S = 2.0735 \text{ kJ/kg}, h_{2s} = 591.8 \text{ kJ/kg}$

State 3: Vapour Saturated, at $P = 0.53 \text{ MPa}$
 $h_3 = 567.081 \text{ kJ/kg}$

State 4: Liquid Saturation, at $P = 0.53 \text{ MPa}$
 $h_4 = 249.59 \text{ kJ/kg}$
 $v_4 = 0.001858 \text{ m}^3/\text{kg}$
 used v_4 , because is approach enthalpy for state 5s

State 5: Efficiency pump equal with Turbine,
 However numerator Isentropic condition and denominatory is actual working.
 $P = 2 \text{ MPa}, T = 310.7 \text{ °K}$
 $h_5 = h_4 + \frac{(h_{5s} - h_4)}{\eta_p} = 249.539 \text{ kJ/kg}$

State 5s: Isentropic pump outlet state;
 $P_{5s} = 2 \text{ MPa}$, Because liquid almost incompressible condition ,
 h_{5s} can be determined. $h_{5s} \approx h_4 + v_4 (P_{5s} - P_4)$
 $= 249.594 \text{ kJ/kg}$

State 6: Liquid Saturation at $P_6 = 2 \text{ MPa}$
 $T_6 = 372.585 \text{ °K}$
 $h_6 = 427.816 \text{ kJ/kg}$

Tabel 9. Thermodynamics State of iso-butane

Working Fluid	Boiling Point, (°C)	P.Cond, (bar)	T. Max, (°C)	P. Max, (bar)	T.C, (°C)	P.C. (bar)
Iso-butane	-11.7	5.03	125	28.9	134.7	3.505
Iso-pentane	27.8	1.45	177	28.87	187.2	0.918
n-pentane	36.1	1.1	186	28.65	196.5	0.683

State	P (Mpa)	T (°K)	S.V (m³/kg)	S (kJ/kg)	h (kJ/kg)
1	2	372.585		2.0735	642.378
2	0.503				591.8
2s	0.503			2.0735	582.875
3	0.503				567.081
4	0.503		0.001858		249.59

5	2	310.7			249.593
5s	2				249.594
6	2	372.585			427.816

The thermodynamic state analysis for iso-butane is shown in Table-7. State 1 is working fluid entering turbine with no fluid droplets with a pressure of 2 Mpa and an enthalpy of 642.378 kJ/kg. State 2 is the actual state of the turbine output with a pressure of 0.503 MPa and enthalpy of 591.8 kJ/kg. Whereas state 2s is the isentropic state of turbine output with pressure of 0.503 Mpa and enthalpy 582.875 kJ/kg. In state 3, the working fluid pressure is 0.503 Mpa and enthalpy 567.081 kJ/kg. The working fluid then enters the feed pump as seen in state 4 with a pressure of 0.503 Mpa and enthalpy of 249.59 kJ/kg. At state 5s, the fluid has pressure of 2

Mpa and enthalpy of 249.593 kJ/kg. In state 5, the actual state of the feedpump and working fluid output enters the heat exchanger with pressure of 2 Mpa and enthalpy of 249.594 kJ/kg. State 6 shows that the working fluid is still in the saturated liquid with a pressure of 2 MPa and enthalpy of 427.816 kJ/kg. The steam returns to the turbine in state 1. This cycle continues to occur at the binary cycle power plant. Thermodynamics State of iso-pentane can follow at Table 10, and than thermodynamic state analysis for n-pentane is shown in Table-11.

Tabel 10. Thermodynamics State of iso-pentane

State	P (Mpa)	T (°K)	S Volume m ³ /kg	Entropi kJ/kg	Enthalpy kJ/kg
1	2	436.98		2.2	740.75
2	0.145				654.21
2s	0.145			2.2	638.94
3	0.145				565.28
4	0.145		0.001662		229.74
5	2	311.68			229.744
5s	2				229.743
6	2	426.98			545.342

The thermodynamic state analysis for iso-pentane is shown in Table 8. State 1 is working fluid entering turbine with no fluid droplets with a pressure of 2 Mpa and an enthalpy of 740.75 kJ/kg. State 2 is the actual state of the turbine output with a pressure of 0.145 MPa and enthalpy of 654.21 kJ/kg. Whereas state 2s is the isentropic state of turbine output with pressure of 0.145 Mpa and enthalpy 638.94 kJ/kg K. In state 3, the working fluid pressure is 0.145 Mpa and enthalpy 565.28 kJ/kg. State 4, working fluid enters the feed

pump with pressure of 0.145 Mpa and enthalpy of 229.74 kJ/kg. At state 5s, the fluid has pressure of 2 Mpa and enthalpy of 229.743 kJ/kg. In state 5, working fluid enters the heat exchanger with pressure of 2 Mpa and enthalpy of 229.744 kJ/kg. State 6 working fluid is still in the saturated liquid with a pressure of 2 MPa and enthalpy of 545.342 kJ/kg. Then the steam returns to the turbine in state 1. This cycle continues to occur at the binary cycle power plant.

Tabel 11. Thermodynamics State of n-pentane

The thermodynamic state analysis for n-pentane is shown in Table-11. State 1 is working fluid entering turbine with a pressure of 2 Mpa and an enthalpy of 689.935 kJ/kg. State 2 is the actual state of the turbine output with a pressure of 0.11 MPa and enthalpy of 592.413 kJ/kg. Whereas state 2s is the isentropic state of turbine output with pressure of 0.11 Mpa and enthalpy

pressure of 2 Mpa and enthalpy of 145.9265 kJ/kg. In state 5, working fluid enters heat exchanger with pressure of 2 Mpa and enthalpy of 145.927 kJ/kg. State 6 shows that the working fluid is still in the saturated liquid with a pressure of 2 MPa and enthalpy of 489.245 kJ/kg. Then the steam returns to the turbine in state 1. This cycle continues to occur at the binary cycle power plant.

575.22 kJ/kg K. In state 3, the working fluid pressure is 0.11 Mpa and enthalpy 499.353 kJ/kg. State 4 working fluid then enters the feed with a pressure of 0.11 Mpa and enthalpy of 145.923 kJ/kg. At state 5s, the fluid has

4.4 Binary Cycle Power Plant Design Optimization

Next is calculating the amount of electricity produced by each of these working fluids. This research will predict considering the critical temperature of the working fluid. The prediction of electrical power is also carried out until the working fluid does not produce electricity anymore. The amount of

State	P(MPa)	T (K)	Specific Volume (m ³ /kg)	Entropy (kJ/kg)	Enthalpy (kJ/kg)
1	2	436.24		1.89	689.935
2	0.11				592.413
2s	0.11			1.89	575.22
3	0.11				499.353
4	0.11		0.001655		145.923
5	2	311.32			145.927
5s	2				145.9265
6	2	436.24			489.245

electrical power generated for each wellhead temperature is attached in Table- 12.

The n-pentane can be used in the brine temperature range of 180.8 °C to 169.4 °C. Below the temperature of 169.4 °C, it is not optimum because n-pentane will not produce electricity. The iso-pentane can be used in the brine temperature range of 163.95 °C to 180.8 °C. Below the temperature of 163.95 °C, it is not optimum because the iso-pentane will not produce electricity.

the planning of a binary cycle power plant for 17 years from 2020 to 2036. Each working fluid will be calculated for how much energy is produced without

Whereas isobutane can generate electricity from a brine temperature of 106.35 °C to 180.8 °C. But below 106.35 °C, isobutane can no longer produce electricity. In Fig. 4, it can be seen that there is a decrease in the 2-phase fluid temperature at

the wellhead and also the brine temperature at the outlet pressure every year by 3°C per year .Figure 5 shows the temperature at which a working fluid is used and produces the amount of electrical power.The n-pentane can be used in the brine temperature range of 180.8 °C to 169.4 °C. Below the temperature of 169.4 °C, it is not optimum because n-pentane will not produce electricity. The iso-pentane can be used in the brine temperature range of 163.95 °C to 180.8 °C. Below the temperature

of 163.95 °C, it is not optimum because the iso-pentane will not produce electricity. Whereas isobutane can generate electricity from a brine temperature of 106.35 °C to 180.8 °C. But below 106.35 °C, isobutane can no longer produce electricity. In Fig. 4, it can be seen that

there is a decrease in the 2-phase fluid temperature at the wellhead and also the brine temperature at the outlet pressure every year by 3°C per year .Figure 5 shows the temperature at which a working fluid is used and produces the amount of electrical pow

will not produce electricity.

Whereas isobutane can generate electricity from a brine temperature of 106.35 °C to 180.8 °C

But below 106.35 °C, isobutane can no longer produce electricity. In Fig. 4, it can be seen that there is a decrease in the 2-phase fluid temperature at the wellhead and also the brine temperature at the outlet pressure every year by 3°C per year .Figure 5 shows the temperature at which a working fluid is used and produces the amount of electrical power. In Fig 5 the condition of each wellhead temperature, iso-butane produces the highest electricity, thus can be used at any temperature, but it will not optimal in a cycle. For this reason, it is necessary to consider the working fluid maximum allowed temperature and critical temperature

Tabel 11. Electric Power Generation by Each Working Fluid Without Considering Tc

Year	Year	Wellhead Temperature (°C)	Inlet Heat Exchanger (Brine) Temperature (°C)	Electric Power Generated (MWh)		
				iso-butane	iso-pentane	n-pentane
1	2020	193	180.8	5.5	3	1.9
2	2021	187	175	5.1	2.2	1
3	2022	182	169.4	4.7	1.4	0.2
4	2023	176	164	4.3	0.7	-
5	2024	171	159	4	-	-
6	2025	166	153.5	3.6	-	-
7	2026	161	148.6	3.2	-	-
8	2027	156	143.7	2.8	-	-
9	2028	151	139	2.5	-	-
10	2029	147	134.5	2.2	-	-
11	2030	142	130	1.9	-	-
12	2031	138	126	1.5	-	-
13	2032	134	121.7	1.2	-	-
14	2033	130	117.7	0.9	-	-
15	2034	126	113.8	0.7	-	-
16	2035	122	110	0.4	-	-
17	2036	119	106	0.1	-	-

The n-pentane can be used in the brine temperature range of 180.8 °C to 169.4 °C. Below the temperature of 169.4 °C, it is not optimum because n-pentane will not produce electricity. The iso-pentane can be used in the brine temperature range of 163.95 °C to 180.8 °C. Below the temperature of 163.95 °C, it is not optimum because the iso-pentane

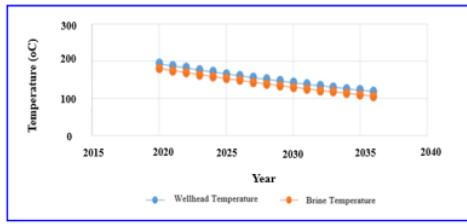


Figure 4. Wellhead and Brine Temperature Drop Each Year

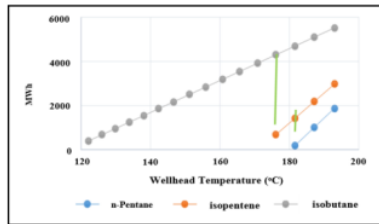


Figure 5. Electric Power Generated by Each Working Fluid

Well output fluid data needs to be corrected by pressure and temperature loss of the fluid flowing in the pipe. The amount of total pressure loss from the manifold to the separator outlet is 3.17 bar and the total temperature loss is 12.2 °C. Fig. 3. shows a decrease in wellhead temperature and brine temperature each year. Optimum working fluid selection is based on the characteristics of working fluid. Heating fluid (brine) temperature must be bigger than working fluid temperature. Each working fluid has the maximum allowable temperature. Other conditions it is also found under a certain temperature, the working fluid does not produce electrical power. Table-12, is shows the optimum working fluid for use at each wellhead temperature.

The optimum n-pentane was used in 1st year with a wellhead temperature of 193 °C, an inlet heat exchanger (brine) temperature of 180.8 °C, and an electric power of 1.9 MWh. The optimum iso-pentane is used in 2nd to 4th years with a wellhead temperature of 176 °C -187 °C, an inlet heat exchanger (brine) temperature of 164 °C -175 °C, and produces electric power of 0.7-2.2 MWh. Whereas the optimum isobutane is used in the 5th to 17th years with a wellhead temperature of 119°C -171°C, an inlet heat exchanger temperature (brine) of 106°C -159°C and the electrical power produced by 0.1- 4 MWh. The Figure 6, as show condition of Wellhead temperature sensitivity for each H-C working fluid.

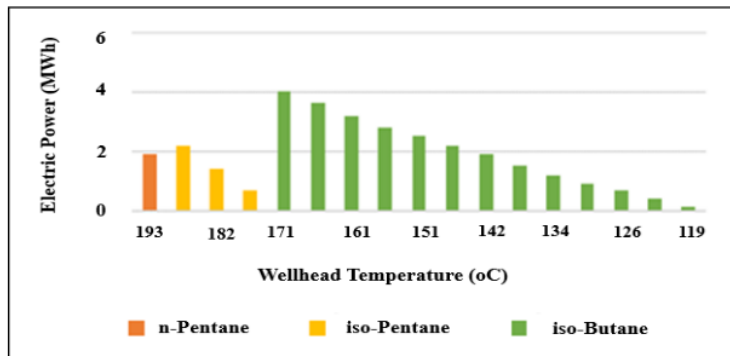


Figure 6. Wellhead Temperature Sensitivity for Each Working Fluid

Tabel 12.
Optimum Working Fluid in Each Wellhead Temperatur

Year	Year	Wellhead T(°C)	Inlet HE (Brine) T(°C)	Working Fluid	Electric Power (MWh)
1	2020	193	180.8	n-pentane	1.9
2	2021	187	175	iso-pentane	2.2
3	2022	182	169.4		1.4
4	2023	176	164		0.7
5	2024	171	159		4
6	2025	166	153.5	iso-butane	3.6
7	2026	161	148.6		3.2
8	2027	156	143.7		2.8
9	2028	151	139		2.5
10	2029	147	134.5		2.2
11	2030	142	130		1.9
12	2031	138	126		1.5
13	2032	134	121.7		1.2
14	2033	130	117.7		0.9
15	2034	126	113.8		0.7
16	2035	122	110		0.4
17	2036	119	106		0.1

6. CONCLUSIONS

So far, the brine water from the separator is only discharged into the environment and can damage the environment due to high temperatures. In this study, an analysis of three types of working fluid used to reheat the brine water was analyzed with the following results. From the predictions for 17 years starting from 2020 to 2036, it was found that the optimum n-pentane is used in 1st year with a wellhead temperature of 193°C and generates electricity of 1.9 MWh. The optimum isopentane is used in 2nd to 4th years with a wellhead temperature of 176-187°C and an electricity of 0.7-2.2 MWh, and the optimum isobutane is used in the 5th to 17th years with a wellhead temperature of 119-171°C and the electricity produced by 0.1- 4 MWh. We can maintain the environment by converting existing energy from brine fluid in separator and it will be used to full fill energy need.

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